

SELECTION OF EFFICIENT MICROBIAL COMMUNITIES: IMPACT OF THE VOLUMETRIC LOAD

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ABSTRACT

Two laboratory-scale (1m high) biofilters were packed with peat and used to treat a complex mixture of VOCs (oxygenated, aromatic and halogenated compounds). A vertical community composition gradient, in terms of both density and diversity, was clearly established and was directly connected to a vertical gradient of biodegradation activities. It is now essential to better understand the complex interactions between microbial community structure and biodegradation functions. Hence, first it appears interesting to consider the selection of efficient microbial communities. This step concerns the activated sludge acclimatization to the VOC mixture. It is realized according to an empiric method and consists in supplying a reactor containing activated sludge with the VOC mixture. The growth of micro-organisms colonizing activated sludge and able to metabolize pollutants is then favored. Does this enrichment step involve a loss of microorganism diversity? Does this loss depend on the concentration of each compound introduced in the reactor? The aim of this research is to evaluate the impact of the applied volumetric load on this acclimatization phase. Two reactors were used and were supplied with a gaseous effluent containing a complex mixture of eleven VOCs with different concentrations. Three different sorts of chemical groups are studied: oxygenated, aromatic and halogenated compounds. Hence, it is essential to measure, as a function of time, the removal of the pollutants in the gas and liquid phases and to link the results obtained to the microbial ecology of this ecosystem in terms of microflora density and diversity. These results will provide interesting information on the removal efficiency of activated sludge and on the potentialities of the treatment system of VOCs using biological processes.

INTRODUCTION

Air pollution control is taken under increasing environmental consideration (Clean Air Act, 1990). Several treatments are being developed in order to treat more accurately Volatile Organic Compounds (VOCs). Among them, biological treatments are an attractive alternative, as its economic and environmental relevance has yet been proved in several applications. A growing number of studies deal with biofiltration and bioscrubbing, but few of them consider a complex mixture removal system. This lack of knowledge in multiple substrates biological elimination systems effectiveness and feasibility is deplorable because, in real case applications, multicomponent pollution is often the rule more than the exception.

In two laboratory-scale (1m high) biofilters packed with peat used to treat a complex mixture of VOCs (oxygenated, aromatic and halogenated compounds), it has been shown that a vertical community composition gradient, in terms of both density and diversity, was clearly established and was directly connected to a vertical gradient of biodegradation activities (Khammar et al., 2005). It is then essential to understand better the complex interactions between microbial community structure and biodegradation functions. It appears interesting to consider more accurately the selection of the efficient microbial communities. It is a crucial step which determines the elimination efficiency level and the reactivity of the bioreactors following the modifications of the gaseous effluent composition. This step concerns the activated sludge acclimatization to the VOCs mixture. It consists on supplying a reactor containing activated sludge with the VOCs mixture. The growth of micro-organisms colonizing activated sludge and able to metabolize pollutants is then favored. Does this enrichment step involve a loss of microorganisms diversity? Does this loss depend on the concentration of each compound introduced in the reactor?

Then, the aim of this work is to evaluate the impact of the applied volumetric load on this acclimatization phase. Two reactors were used and were supplied with a gaseous effluent containing a complex mixture of eleven VOCs for which the concentration differs.

The microbial communities were monitored according to the following parameters: pollutant elimination efficiency, bacterial density and the structure of the microbial communities. The structure of bacterial communities has been approached by using the Single Strand Conformation Polymorphism (SSCP) method (Orita et al. 1989). This technique has been adapted to study the bacterial diversity of ecosystems by the amplification of the 16S rDNA part (Lee et al. 1996; Schwieger and Tebbe. 1998).

MATERIALS AND METHODS

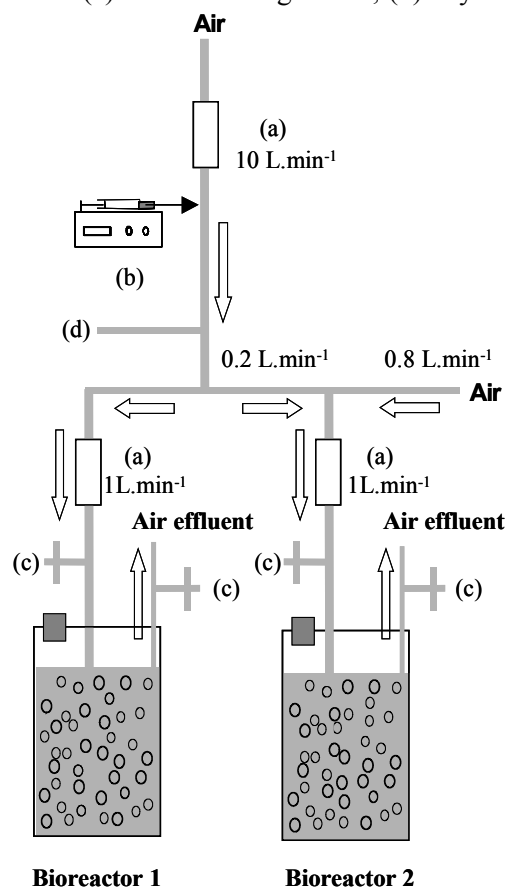
The VOC Mixture

The mixture of VOCs contained 11 compounds divided in respectively oxygenated compounds with methanol, acetone, methyl ethyl ketone (MEK), methyl isobutyl ketone (MIBK), butyl and ethyl acetates (BA, EA), aromatic compounds with toluene, ethylbenzene, p-xylene and halogenated compounds with dichloromethane (DCM) and 1,2-dichloroethane (DCE) (Carlo Erba Reagenti, 99% puro). The pollutants mixture was prepared by mixing equal masses of the above VOCs.

Reactor design

Figure 1 shows the pilot scale units used in this study. Each unit consisted of a glass reactor. The liquid VOCs mixture was continuously injected and vaporized into an air stream operating at $10 \text{ L}\cdot\text{min}^{-1}$ via a Precidor syringe pump (Infors AG, Switzerland). Some of the polluted air ($1 \text{ L}\cdot\text{min}^{-1}$) was forced through a 5 L reactor seeded with 4 L of activated sludge sampled from a domestic sewage treatment plant. The experiment was performed at normal room temperature ($20\text{-}25^\circ\text{C}$).

Figure 1: Pilot scale units. (a) : flow rate regulators; (b) : syringe pump loaded with the mixture of 11



VOCs; (c) : gas sampling; (d): gas split.

The concentration of each compound in the inlet gas stream was 700 and 140 mg.m⁻³ for reactors 1 and 2 respectively. The applied volumetric loads were then 115.5 and 23.1 g VOCs.h⁻¹.m⁻³ activated sludge for bioreactors 1 and 2 respectively. Both reactors have been monitored for 38 days.

Biodegradation Monitoring

The biodegradation of VOCs was measured daily by monitoring the concentration of each compound at the sampling inlets and outlets. The reactor sampling points were directly connected to a gas chromatograph unit (HP 6890, Hewlett Packard) equipped with a flame ionization detector. The analysis conditions are summarized in Table 1.

The biodegradation was monitored by calculating the VOCs removal efficiency (RE). The Relative Standard Deviation (RSD) has been estimated at 10% (n = 9 replicates).

Injector	Oven and chromatographic column	Detector
Temperature: 150°C	Temperature Ramp: 40°C —————▶ 90°C —————▶ 150°C 1 min 15°C.min ⁻¹ 4 min 10°C.min ⁻¹	Temperature: 220°C
	Column HP-1 (polydimethylsiloxane)	Air flow rate: 310 mL.min ⁻¹
	He flow rate (carrier gas) : 2,5 mL. min ⁻¹	H ₂ flow rate: 46.5 mL.min ⁻¹
		He flow rate: 30 mL.min ⁻¹

Table 1: Chromatographic conditions

Bacterial Enumeration

Bacteria were enumerated by fluorescence microscopy using staining with DAPI (4',6-diamidino-2-phenylindole, Sigma, USA) to determine the total bacteria number (Kepner and Pratt, 1994).

A volume of sample (2 mL) was diluted in 9 volumes of 1% sodium hexametaphosphate, and homogenized with a blender (Ultra Turax, T25 basic, IKA) during 2 min at 19000 revolutions per min. Then, 1mL of this suspension was incubated with 3.7% formaldehyde during 30 min, before counter-staining by DAPI at a final concentration of 20 µg.mL⁻¹ during 1 h, in the dark, at an agitation of 200 rpm.

Stained bacteria were recovered on 0.2 µm-polycarbonate membrane filter (Millipore GTBP, Ireland) by microfiltration. The filters were then mounted on microscope slides in Mounting Medium (Sigma, USA) and observed using an epifluorescence microscope (DMLB, Leica, Germany) equipped with a blue excitation filter (BP 340-380 nm) and an LP 425barrier filter. For each slide, 30 fields were counted. The ability of the data was expressed in term of Relative Standard Deviation (RSD).

Analysis of total DNA by PCR-SSCP

The DNA extraction method has previously been described (Godon *et al.*, 1997). The target DNA amplified was the V3 region of the 16S rDNA gene for the bacteria domain (primers W104 and W049) (Table 2). Primer W104 was labeled by a 6-FAM fluorochrome. Each reaction tube contained 100 ng of each primer, 10 mM dNTPs, 1X Pfu Turbo DNA polymerase reaction buffer with 25 mM MgCl₂, 1.25 U Pfu Turbo DNA polymerase (Stratagene) and 1 µL of purified template DNA adjusted to a total volume of 50 µL.

Name	Sequence	Position*
W104	5'-6-Fam -TTACCGCGGCTGCTGGCAC-3'	R533
W049	5'-ACGGTCCAGACTCCTACGGG-3'	F331

Table 2: Primers used to amplify the 16S rDNA and their characteristics.* positions were defined by the *E. coli* sequence

The reaction mixtures were placed in a thermocycler (Perkin Elmer) at 94°C for 30 s. Three-stage cycles were then performed 30 times: at 94°C for 30 s, at 61°C for W104/W49 for 30 s, 72°C for 30 s, and a final stage at 72°C for 15 min.

The PCR products were diluted depending on the band intensity on the 2% agarose gel. A 1 µL of diluted PCR products was mixed with 18.8 µL of loading buffer TSR (Applied Biosystem) and 0.2 µL of internal weight standard Genescan-400 HD Rox (Applied Biosystem). The double-strand helix was then separated for 2 min at 94°C, and immediately cooled in an ice-water bath for 10 min, ensuring that single-stranded products were obtained. Capillary electrophoresis S.S.C.P analysis was performed on an ABI PRISM 310 automated DNA sequencer (Applied Biosystem) equipped with a capillary tube filled with a polymer, for 30 min at 12 KV and a 32°C temperature. A sample volume of 5 µL was loaded onto the polymer [Genescan polymer (7% w/w) at 8 mg.mL⁻¹, Glycerol 10%, TBE 1X].

The SSCP profiles were compared after alignment with the internal weight standard.

The analysis of SSCP profiles is realized in a first time by visual comparison, then by using the SSCP2 software developed in the Environmental Biotechnology Laboratory, Narbonne, France. This software determines and aligns peaks; so co-migrated peaks were recognized.

RESULTS AND DISCUSSION

Two parallel bioreactors, 1 and 2 were designed to run under identical operating conditions (Figure 1). Each reactor was supplied with a complex synthetic gaseous effluent containing oxygenated, aromatic and chlorinated compounds but the concentration differed. The concentration of each pollutant was 700 mg.m⁻³ and 140 mg.m⁻³ for bioreactor 1 and 2 respectively. Pollutant removal, dynamics of microbial densities and microbial diversity were monitored in function of time.

Pollutant removal for bioreactors 1 and 2

Figure 2 presents the VOCs removal efficiencies, expressed in percentages, for both bioreactors 1 and 2.

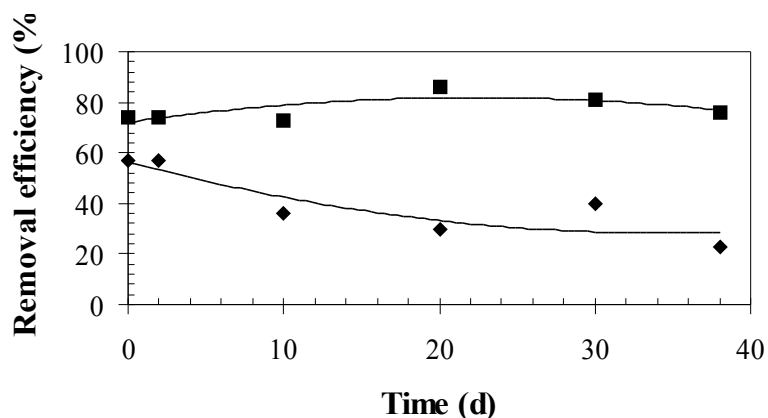


Figure 2: Removal of VOCs for both bioreactors as a function of time. ▲ Bioreactor 1, ■ Bioreactor 2, — polynomial curve (order 2).

For bioreactor 1, the removal efficiency measured decreased from 60% to 30% at $t = 26$ day. The abatement remained stable until $t = 38$ day. For bioreactor 2, the removal efficiency remained close to 80% from the beginning to $t = 38$ day.

Table 3 presents the removal efficiencies obtained for oxygenated, aromatic and chlorinated compounds for both bioreactors.

Compounds	Bioreactor 1	Bioreactor 2
Oxygenated	45	100
Aromatic	NR	55
Chlorinated	NR	50

Table 3: Elimination efficiency (%) reached for VOCs chemical groups. NR: Not Removed.

For bioreactor 1, the oxygenated compounds were removed and the elimination efficiency reached 45% while for bioreactor 2, oxygenated compounds were completely eliminated and the abatement of aromatics and halogenated compounds reached 55 and 50% respectively.

All members of each family behaved similarly for bioreactor 2. For bioreactor 1, the esters were completely removed while the abatement of MEK, methanol, and acetone and MIBK decreased from values close to 100% at the beginning of the experiment to 30%, 25% and 0% respectively at $t = 38$ day.

A better elimination efficiency is reached when the bioreactor was acclimatized with the complex VOCs mixture at low concentration. Moreover, different chemical families of compounds are removed.

Quantitative Microbial Dynamics

The colonization dynamics were monitored as a function of time for 38 days (Figure 3). The results obtained by enumerating total bacteria stained with DAPI show that the bacterial densities followed the same evolution. The number of total bacteria reached at $t = 36$ day remains similar: $1.4 \cdot 10^9$ and $7.7 \cdot 10^8$ cells.mL⁻¹ for bioreactor 1 and 2 respectively.

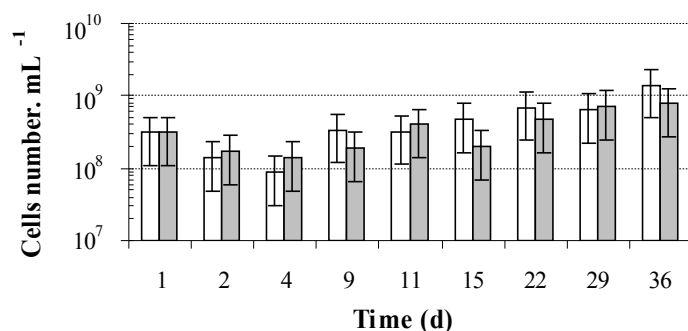


Figure 3: Colonisation dynamics for both bioreactors. □ Bioreactor 1; ■ Bioreactor 2.

The applied volumetric load seems to have an impact on the removal of compounds in terms of elimination efficiency and chemical nature of the biodegraded chemicals without having an influence on the densities of the total bacterial community.

Structure of Total Bacterial Communities

The SSCP method was used to define the structure of total bacterial diversity at the dominant level in activated sludge samples collected as a function of time for both bioreactors (Figure 4).

On a given SSCP pattern, each peak corresponds to a distinct 16S rDNA molecule. SSCP profile analysis at the beginning of the experiment ($t = 0$) reveals 25 peaks. Between $t = 0$ to $t = 38$ days, the evolution of the genetic structure differs for both bioreactors. For bioreactor 1, the SSCP analysis of total bacterial DNA extracted from samples reveals 15 dominant peaks for which 10 peaks are dominant on the left of the pattern while for bioreactor 2, the number of peaks remains stable and no dominant peak is counted. Hence, at $t = 38$ day, the SSCP patterns obtained for both reactors are different.

A simplification of the genetic structure of the total bacterial community is then observed for bioreactor 1 supplied with the highest volumetric load. Moreover, a dominant bacterial community appears.

In return, when the bioreactor was supplied with the VOCs complex mixture at low concentration, a large bacterial diversity is kept.

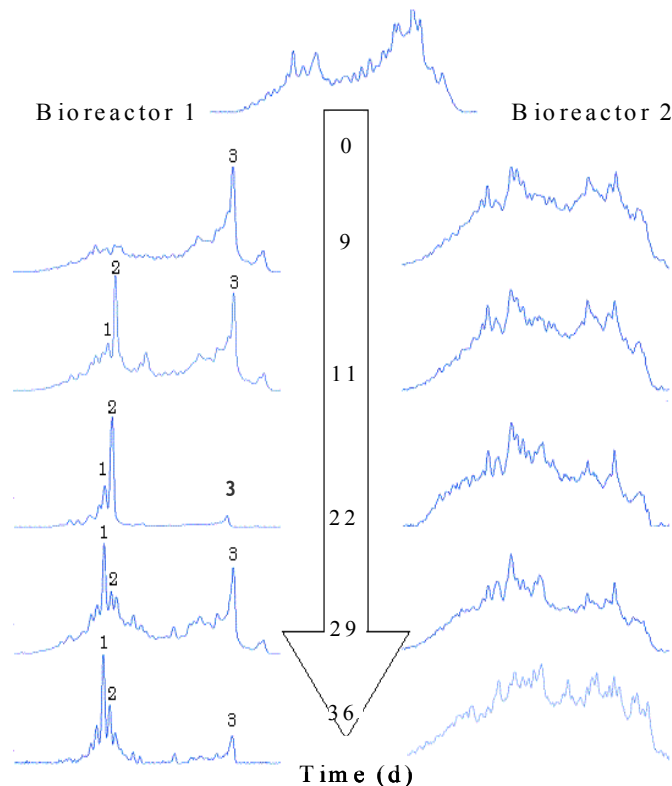


Figure 4: Bacterial community dynamics for bioreactors 1 and 2

Conclusion

This work highlights that the applied volumetric load seems to influence the functioning and the genetic structure of the bacterial community during the acclimatization phase.

-A high volumetric load seems to induce a low effective functioning in terms of elimination efficiency and chemical nature of removed compounds, and a simplification of the genetic structure of the total bacterial community with the apparition of a dominant microflora.

-A low volumetric load seems to favour a more efficient functioning and allows a wealthier bacterial diversity to be kept.

-In these biological systems treating a complex mixture of VOCs, the obtained results would show, in term of microbial ecology, that a good functioning seems to be correlated with the high level of the bacterial diversity and the absence of a dominant bacterial community.

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